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## FUEL DATA FOR COMBUSTION WITH AIR

| Fuel              | Formula (state)  | Density<br>[kg/m <sup>3</sup> ] | Theoretical<br>air/fuel ratio       | Higher<br>Heating<br>Value<br>[MJ/kg] | Maximum<br>adiabatic<br>combustion $T$<br>[K] | Flash point<br>& Autoignition<br>temperature <sup>a</sup><br>[K] | Ignition<br>limits <sup>b</sup> | Laminar<br>deflagration<br>speed (max.)<br>[m/s] |
|-------------------|--|---------------------------------|-------------------------------------|---------------------------------------|---|--|---------------------------------|--|
| Acetylene         | C <sub>2</sub> H <sub>2</sub> (g)                            | 1.1                             | 11.9 m <sup>3</sup> /m <sup>3</sup> | 48                                    | 2500*   | <180, 600  | 2.5..100                        | 1.5  |
| Benzene           | C <sub>6</sub> H <sub>6</sub> (l)                            | 880                             | 13.3 kg/kg                          | 42.3                                  | 2400  | 262, 840   | 1.5..7.5                        | 1.1  |
| Bio-diesel        | C <sub>17</sub> H <sub>32</sub> O <sub>2</sub> (l) esters    | 880                             | 12.4 kg/kg                          | 40                                    | -   | 420, -   |                                 |  |
| Bio-petrol        | C <sub>6</sub> H <sub>14</sub> O(l) Ethyl Tert. Butyl Ether  | 750                             | 12.2 kg/kg                          | 36                                    | -   | -  |                                 |  |
| n-Butane          | C <sub>4</sub> H <sub>10</sub> (g)                           | 2.4                             | 31 m <sup>3</sup> /m <sup>3</sup>   | 49.5                                  | 2250  | 210, 670   | 1.5..9.3                        | 0.45   |
| iso-Butane        | C <sub>4</sub> H <sub>10</sub> (g)                           | 2.4                             | 31 m <sup>3</sup> /m <sup>3</sup>   | 49.5                                  | 2250  | 190, 710   | 1.6..8.4                        | 0.45   |
| Carbon (graphite) | C(s)   | 2250                            | 11.5 kg/kg                          | 33                                    |   | 600, 670   |                                 |  |
| Carbon monoxide   | CO(g)  | 1.2                             | 2.4 m <sup>3</sup> /m <sup>3</sup>  | 10                                    | 2400  | -, 900   | 12..75                          | 0.20   |
| Coal (dry, mean)  | 85%C5%H5%O5%M(s) <sup>c</sup>                                | 1300..1400                      | 10 kg/kg                            | 31                                    | 2200  | 550, 600   |                                 |  |
| Diesel or Gas-oil | 87%C13%H(l) <sup>d</sup>                                     | 820..860                        | 14.5 kg/kg                          | 47                                    |   | 330, 480   | 0.6..8                          |  |
| DME               | C <sub>2</sub> H <sub>6</sub> O(g) (dimethyl ether)          | 1.8                             | 14.3 m <sup>3</sup> /m <sup>3</sup> | 30                                    |   | 232, 600   | 3.4..20                         | 0.40   |
| ETBE              | C <sub>6</sub> H <sub>14</sub> O(l) (ethyl tert-butyl ether) | 770                             | 12.2 kg/kg                          | 43                                    |   | 248, 580   | 1.4..10                         |  |
| Ethane            | C <sub>2</sub> H <sub>6</sub> (g)                            | 1.2                             | 16.7 m <sup>3</sup> /m <sup>3</sup> | 51.9                                  | 2100  | 140, 800   | 3.0..15                         | 0.40   |
| Ethanol           | C <sub>2</sub> H <sub>6</sub> O(l)                           | 790                             | 9.0 kg/kg                           | 29.7                                  | 2200  | 285, 630   | 3.3..21                         | 0.80   |
| Ether             | C <sub>4</sub> H <sub>10</sub> O(l) (diethyl ether)          | 715                             | 11.2 kg/kg                          | 37.2                                  |   | 230, 440   | 1.8..37                         |  |
| Fuel-oil          | 84%C10%H3%S1%N2%H2O(l) <sup>e</sup>                          | 850..990                        | 15 kg/kg                            | 44                                    | 2200  | 320, 480   | 0.7..5                          |  |
| Gasoline          | 85%C15%H(l) <sup>f</sup>                                     | 730..760                        | 14.7 kg/kg                          | 48                                    | 2200  | 230, 650   | 1.3..8                          | 0.35   |
| n-Hexadecane      | C <sub>16</sub> H <sub>34</sub> (l)                          | 773                             | 14.9 kg/kg                          | 47.3                                  | 2200  | 400, 475   | 0.5..4.7                        |  |
| n-Heptane         | C <sub>7</sub> H <sub>16</sub> (l)                           | 685                             | 15.2 kg/kg                          | 48.1                                  | 2200  | 269, 560   | 1.1..6.7                        | 0.40   |

|                     |   |            |                                     |      |      |          |          |      |
|---------------------|---|------------|-------------------------------------|------|------|----------|----------|------|
| Hydrogen            | H <sub>2</sub> (g)                              | 0.08       | 2.4 m <sup>3</sup> /m <sup>3</sup>  | 142  | 2400 | -, 850   | 4.0..75  | 3.5  |
| Kerosene Jet A-1    | 85%C15%H(l) <sup>g</sup>                        | 780..840   | 15 kg/kg                            | 47   | 2300 | 330, 500 | 0.7..6   | 0.20 |
| Methane             | CH <sub>4</sub> (g)                             | 0.67       | 9.5 m <sup>3</sup> /m <sup>3</sup>  | 55.5 | 2200 | 85, 850  | 4.5..16  | 0.45 |
| Methanol            | CH <sub>4</sub> O(l)                            | 790        | 6.5 kg/kg                           | 22.7 | 2150 | 285, 680 | 6.0..37  | 0.50 |
| Natural gas         | CH <sub>4</sub> (g) <sup>h</sup>                | 0.68..0.70 | 9.5 m <sup>3</sup> /m <sup>3</sup>  | 54   | 2250 | -, 850   | 5.3..15  | 0.45 |
| n-Octane            | C <sub>8</sub> H <sub>18</sub> (l)              | 703        | 15 kg/kg                            | 47.9 | 2300 | 286, 500 | 1..6     | 0.40 |
| iso-Octane          | C <sub>8</sub> H <sub>18</sub> (l) <sup>i</sup> | 690        | 15 kg/kg                            | 47.9 | 2300 | 261, 690 | 1..6     | 0.40 |
| Propane             | C <sub>3</sub> H <sub>8</sub> (g)               | 1.8        | 23.8 m <sup>3</sup> /m <sup>3</sup> | 50.0 | 2250 | 170, 750 | 2.0..9.5 | 0.45 |
| Propylene           | C <sub>3</sub> H <sub>6</sub> (g)               | 1.8        | 21.4 m <sup>3</sup> /m <sup>3</sup> | 48.9 | -    | -        | 2.4..11  | -    |
| Wood<br>(dry, mean) | 50%C5%H45%O(s) <sup>j</sup>                     | 500..1000  | 5.6 kg/kg                           | 20   | 2100 | 550, 700 | -        | -    |

All data for combustion with air, at 298 K and 100 kPa. Additional data in [Wiki](#).

\*Maximum adiabatic combustion temperature for the oxyacetylene torch 3400 K.

<sup>a</sup>Flash point: minimum temperature for spark ignition near the condensed phase. Autoignition: minimum temperature for self ignition (without spark).

<sup>b</sup>% by volume of gaseous fuel in the mixture with air.

<sup>c</sup>% by weight, dry bituminous coal; C refers to total carbon content (fixed plus volatile matter), M refers to inert matter.

<sup>d</sup>% by weight; diesel or gas-oil is a distilled mixture with  $M=0.17..0.20$  kg/mol,  $T_b=470..530$  K (10% and 90% boiled),  $p_v(38\text{ }^\circ\text{C})=0.7$  kPa,  $\nu<4\times 10^{-6}$  m<sup>2</sup>/s at 55 °C (the flash point of diesel), 50..55 cetane number, and sulfur content <500 ppm, that may be approximated by C<sub>12</sub>H<sub>26</sub> (n-Dodecane). Cetane is n-hexadecane, C<sub>16</sub>H<sub>34</sub>. As for most hydrocarbons, the solubility in water is negligible, and it may be carcinogen.

<sup>e</sup>% by weight; fuel-oils are mixtures of residues and heavy fraction distillates (and maybe used and waste oils), with sulfur content <0.5%, and may be approximated by C<sub>14</sub>H<sub>26</sub>. Pour points are usually below 0 °C for distillates and below 20 °C for residuals, but they are heated for handling.

<sup>f</sup>% by weight; gasoline is a distilled mixture with  $M=0.10..0.12$  kg/mol,  $T_b=300..440$  K (10% and 90% boiled),  $p_v(38\text{ }^\circ\text{C})=60$  kPa for the summer blend and  $p_v(40\text{ }^\circ\text{C})=90$  kPa for the winter blend, 90..100 motor octane number, and sulfur content <300 ppm, that may be approximated by C<sub>7</sub>H<sub>17</sub> or C<sub>8</sub>H<sub>18</sub> (iso-octane), except for the vapour pressure. Composition differences yield a wide scatter in property values; e.g. the flash point may range from -230 K to 240 K, autoignition temperature from 550 K to 750 K.

<sup>g</sup>% by weight; kerosene (or kerosene) is a distilled mixture with  $T_b=450..600$  K (10% and 90% boiled),  $T_f=-40$  °C,  $\nu=8\times 10^{-6}$  m<sup>2</sup>/s at -20 °C, that may be approximated by n-dodecane (C<sub>12</sub>H<sub>26</sub>) or 1-dodecene (C<sub>12</sub>H<sub>24</sub>). Commercial (Jet A-1, Jet A, and Jet B) and military (JP-4, JP-5, JP-8...) jet propulsion fuels, are basically mixtures of kerosene and gasoline (half-&-half for JP-4, 99.5% kerosene for JP-5 and JP-8, 100% kerosene for Jet A-1), plus special additives (1..2%): corrosion inhibitor, anti-icing, and anti-static compounds. Jet A-1 is the international jet fuel with  $T_f=-50$  °C (-47 °C as a limit); Jet A (with  $T_f=-40$  °C) is a low-grade Jet A-1 only and mostly used in USA; and Jet B ( $T_f<-50$  °C), the commercial name of JP-4, is only used in very cold climates. They all have a lower heating value of 42.8..43.6 MJ/kg. Minimum flash point is 60 °C for JP-5, 38 °C for Jet A-1 and JP-8 (Jet A-1 typical value is 50 °C, with a vapour pressure at this point of 1.5 kPa; 1 kPa at 38 °C), and -20 °C for JP-4. Typical density at 15 °C is 810 kg/m<sup>3</sup> for Jet A-1, and 760 kg/m<sup>3</sup> for Jet B.

<sup>h</sup>Natural gas is a mixture with some 90% methane,  $M=0.017..0.019$  kg/mol,  $T_b=110..120$  K (10% and 90% boiled) and 120 motor octane number.

<sup>i</sup>Isooctane or trimethylpentane,  $T_f=166$  K,  $T_b=372$  K,  $c=2200$  J/(kg×K), Motor Octane Number MON=100.

<sup>j</sup>% by weight; wood is basically cellulose, a long polysaccharide (C<sub>6</sub>H<sub>10</sub>O<sub>5</sub>)<sub>n</sub> with  $n=5000..10000$  and  $M=500..10000$  kg/mol.